

ME444 ENGINEERING PIPING SYSTEM DESIGN

CHAPTER 1: INTRODUCTION

TENTATIVE SCHEDULE

- BEFORE MIDTERM: THEORY OF FLOW IN PIPE, PIPE SIZING, PIPING MATERIALS, PUMP SELECTION
- AFTER MIDTERM: DESIGN OF VARIOUS PIPING SYSTEMS FOR BUILDINGS AND INDUSTRIES

Web: <http://dulyachot.me.engr.tu.ac.th/me444/me444.htm>



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1. INTRODUCTION
2. STANDARDS
3. BASIC UNITS
4. BASIC FLOW IN PIPE
5. QUICK LOOK AT PIPE DRAWINGS

1. INTRODUCTION



PIPING SYSTEMS EXIST IN EVERY ENGINEERING APPLICATION.

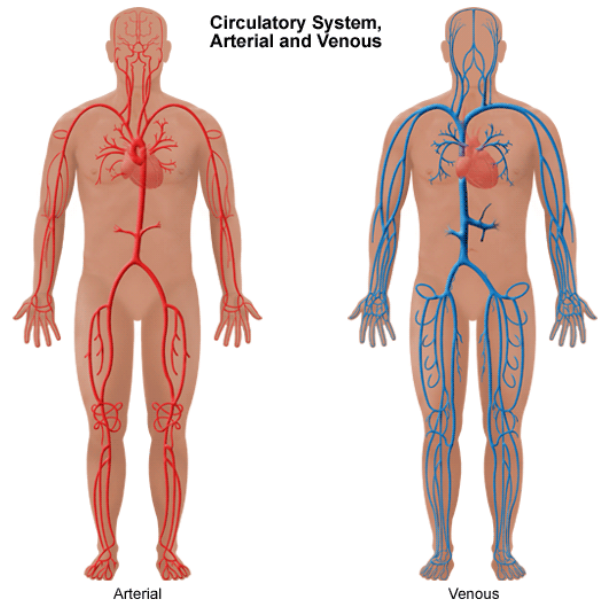
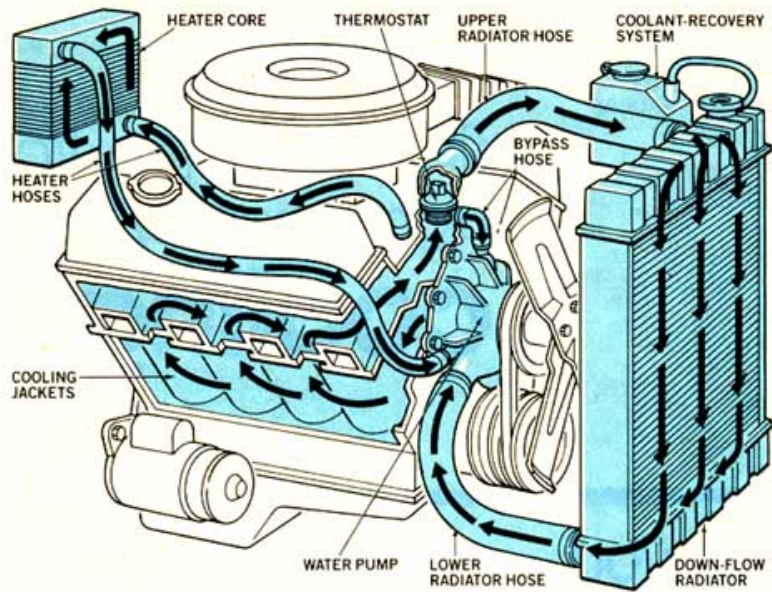
APPLICATIONS:

PLUMBING, FIRE PROTECTION, PROCESS, AIR-CONDITIONING, REFRIGERATION, VENTILATION, COMPRESSED GAS, STEAM

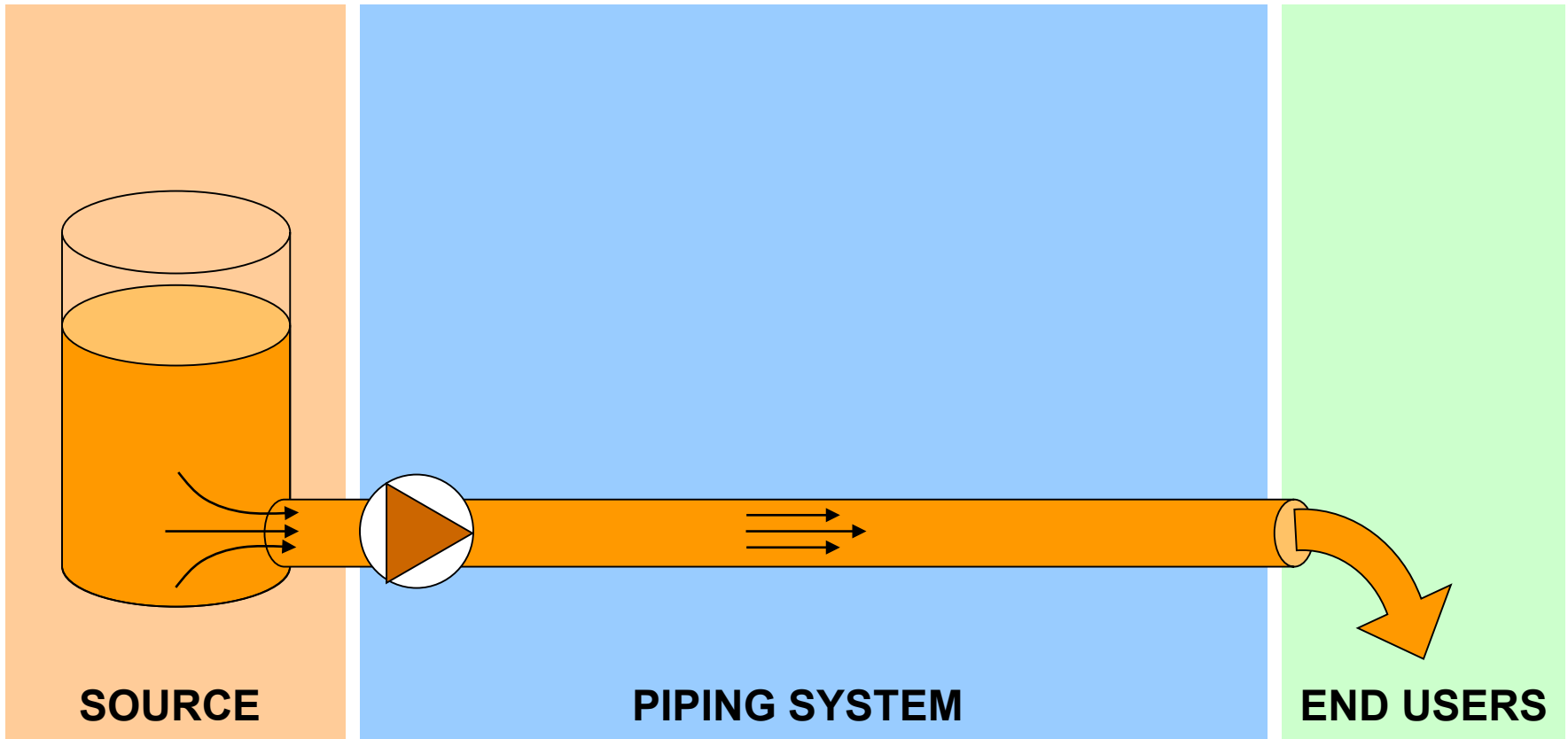


FUNCTION:

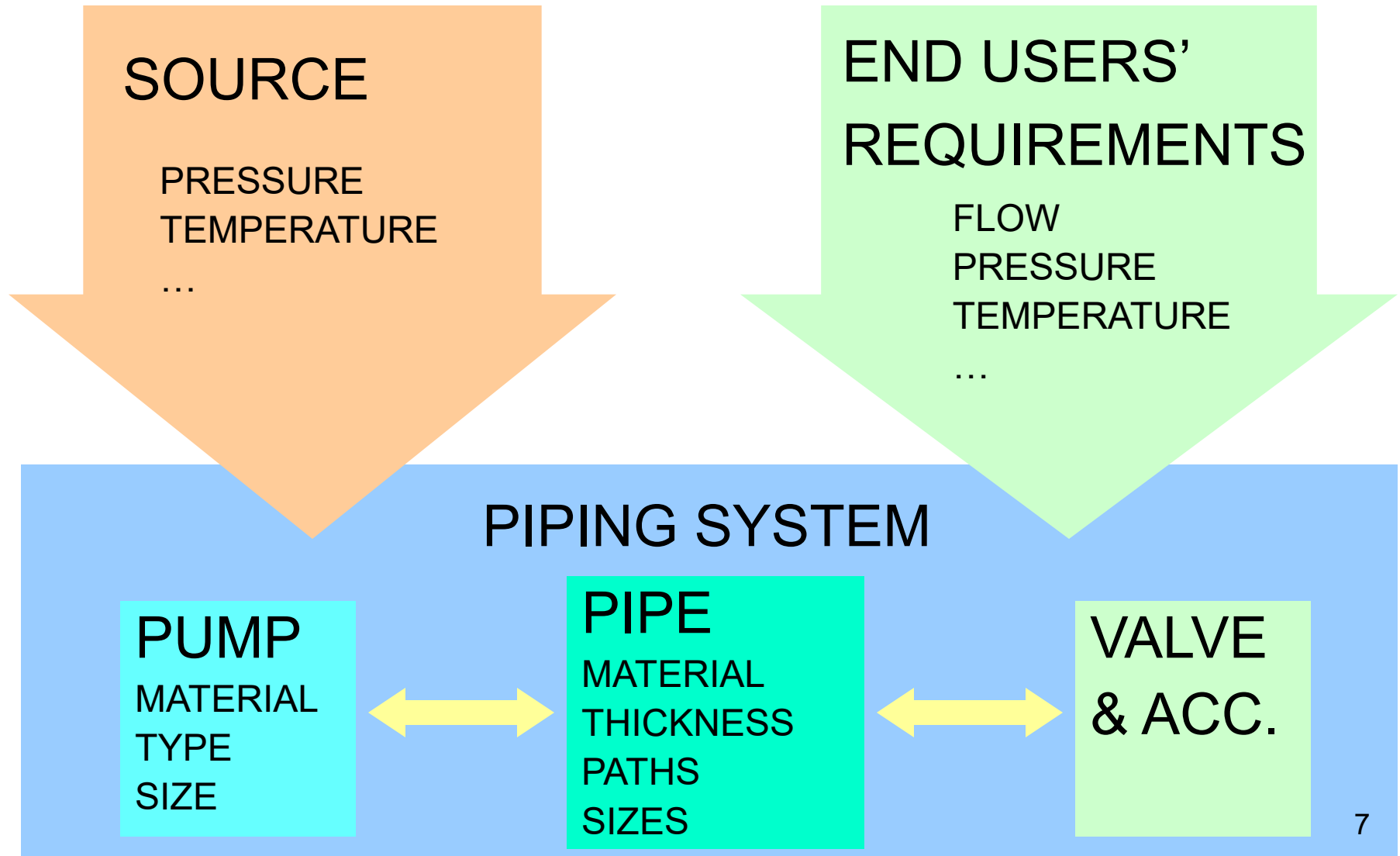
TRANSMIT FLUID AT A PREFERRED RATE TO THE DESTINATIONS WITH PREFERRED PROPERTIES (I.E. PRESSURE, TEMPERATURE)



DESIGN CONCEPT



PIPING SYSTEM DESIGN



2. STANDARDS



American National Standard Institute (ANSI)



American Petroleum Institute (API)



American Society of Heating, Refrigerating and Air-Conditioning Engineers (ASHRAE)



American Society of Mechanical Engineers (ASME)

ASME STANDARDS

B31.1. Power Piping

B31.2. Fuel Gas Piping

B31.3. Process Piping

B31.4. Pipeline Transportation Systems for Liquid Hydrocarbons
and Other Liquids

B31.5. Refrigeration Piping

B31.8. Gas Transmission and Distribution Piping

B31.9. Building Services Piping

B31.11. Slurry Transportation Piping

STANDARDS



American Society of Testing and Materials (ASTM)



International Organization for Standardization (ISO)



American Water Works Association (AWWA)



National Sanitation Foundation (NSF)

STANDARDS



National Fire Protection Association (NFPA)



Factory Mutual Research Corporation (FM)



Underwriters Laboratories (UL)

STANDARDS



British Standard



Deutsches Institut für Normung



Japanese Industrial Standard



Old mark
(expired)



วิศวกรรมสถานแห่งประเทศไทย ในพระบรมราชูปถัมภ์

3. BASIC UNITS

PIPE SIZE: INCHES, mm.

PIPE LENGTH: FEET, METRES

VOLUME: CU.M., CU.FT., LITRES, GALLONS

FLOWRATE: GPM, CU.M./H, LPS, LPM, CFM

PRESSURE: PSI, BAR, m.WG., KG/CM^2

POWER: KW, HP

STUDENTS MUST HAVE THE CONVERSION FACTORS

7 basic quantities

ปริมาณ	หน่วยวัดในระบบเอสไอ	ตัวย่อ
ความยาว	เมตร	m
มวล	กิโลกรัม	kg
เวลา	วินาที	s
กระแสไฟฟ้า	แอมแปร์	A
อุณหภูมิ	เคลวิน	K
ปริมาณของสาร	โมล	m
ความส่องสว่าง	แรงเทียน (candela)	cd

Basic conversion

Length

1 in (inch) = 25.4 mm = 2.54 cm = 0.0254 m = 0.08333 ft

1 ft (foot) = 0.3048 m

1 m (meter) = 3.2808 ft = 39.37 in

1 km = 0.6214 mile = 3281 ft

Mass

1 kg = 1,000 g = 2.2046 lb

1 lb = 16 oz = 0.4536 kg =

Temperature

celsius, rankine, kelvin, centigrade, fahrenheit,

- $1^{\circ}\text{C} = 1.8^{\circ}\text{F}$
- $1^{\circ}\text{F} = 0.555^{\circ}\text{C}$
- 0°C corresponds to 32°F , 273.16 K and 491.69 R
- $T(^{\circ}\text{R}) = (9/5)T(\text{K})$
- $T(^{\circ}\text{F}) = [T(^{\circ}\text{C})](9/5) + 32$
- $T(^{\circ}\text{F}) = [T(\text{K}) - 273.15](9/5) + 32$
- $T(^{\circ}\text{C}) = 5/9[T(^{\circ}\text{F}) - 32]$

Area

Length

$$1 \text{ in (inch)} = 25.4 \text{ mm} = 2.54 \text{ cm} = 0.0254 \text{ m} = 0.08333 \text{ ft}$$

$$1 \text{ ft (foot)} = 0.3048 \text{ m}$$

$$1 \text{ m (meter)} = 3.2808 \text{ ft} = 39.37 \text{ in}$$

$$1 \text{ km} = 0.6214 \text{ mile} = 3281 \text{ ft}$$

Mass

$$1 \text{ kg} = 1,000 \text{ g} = 2.2046 \text{ lb}$$

$$1 \text{ lb} = 16 \text{ oz} = 0.4536 \text{ kg} =$$

Volume

barrel, gallon, cubic centimeter (cm^3), cubic feet (foot^3), cubic inch (inch^3), cubic meter (meter^3), cubic yard (yard^3), quarts, liters, acre foot, board foot, bushel, cord, cup, dram, fluid ounce, peck, pint, quart, tablespoon, teaspoon,

- 1 Gallon (U.S.) = $3.785 \times 10^{-3} \text{ m}^3 = 3.785 \text{ dm}^3$ (liter) = $0.13368 \text{ ft}^3 = 4.951 \times 10^{-3} \text{ yd}^3 = 0.8327$
Imp. gal (UK) = 4 Quarts = 8 Pints
- 1 Imp. gal (UK) = $4.546 \times 10^{-3} \text{ m}^3 = 4.546 \text{ dm}^3 = 0.1605 \text{ ft}^3 = 5.946 \times 10^{-3} \text{ yd}^3 = 1.201 \text{ gal}$
(US)
- 1 dm^3 (Liter) = $10^{-3} \text{ m}^3 = 0.03532 \text{ ft}^3 = 1.308 \times 10^{-3} \text{ yd}^3 = 0.220 \text{ Imp gal (UK)} = 0.2642$
Gallons (US) = 1.057 Quarts = 2.113 Pints
- $1 \text{ ft}^3 = 0.02832 \text{ m}^3 = 28.32 \text{ dm}^3 = 0.03704 \text{ yd}^3 = 6.229 \text{ Imp. gal (UK)} = 7.481 \text{ gal (US)} =$
1,728 Cu.In.

Volume Flowrate

- $1 \text{ m}^3/\text{h} = 2.7778 \times 10^{-4} \text{ m}^3/\text{s} = 0.2778 \text{ dm}^3(\text{litre})/\text{s} = 9.810 \times 10^{-3} \text{ ft}^3/\text{s} = 0.5886 \text{ ft}^3/\text{min} (\text{cfm}) = 3.667 \text{ Imp.gal (UK)}/\text{min} = 4.403 \text{ gal (US)}/\text{min}$
- $1 \text{ gal (US)}/\text{min} = 6.30888 \times 10^{-5} \text{ m}^3/\text{s} = 0.227 \text{ m}^3/\text{h} = 0.06309 \text{ dm}^3(\text{litre})/\text{s} = 2.228 \times 10^{-3} \text{ ft}^3/\text{s} = 0.1337 \text{ ft}^3/\text{min} = 0.8327 \text{ Imperial gal (UK)}/\text{min}$
- $1 \text{ ft}^3/\text{min} = 1.7 \text{ m}^3/\text{h} = 0.47 \text{ l/s}$

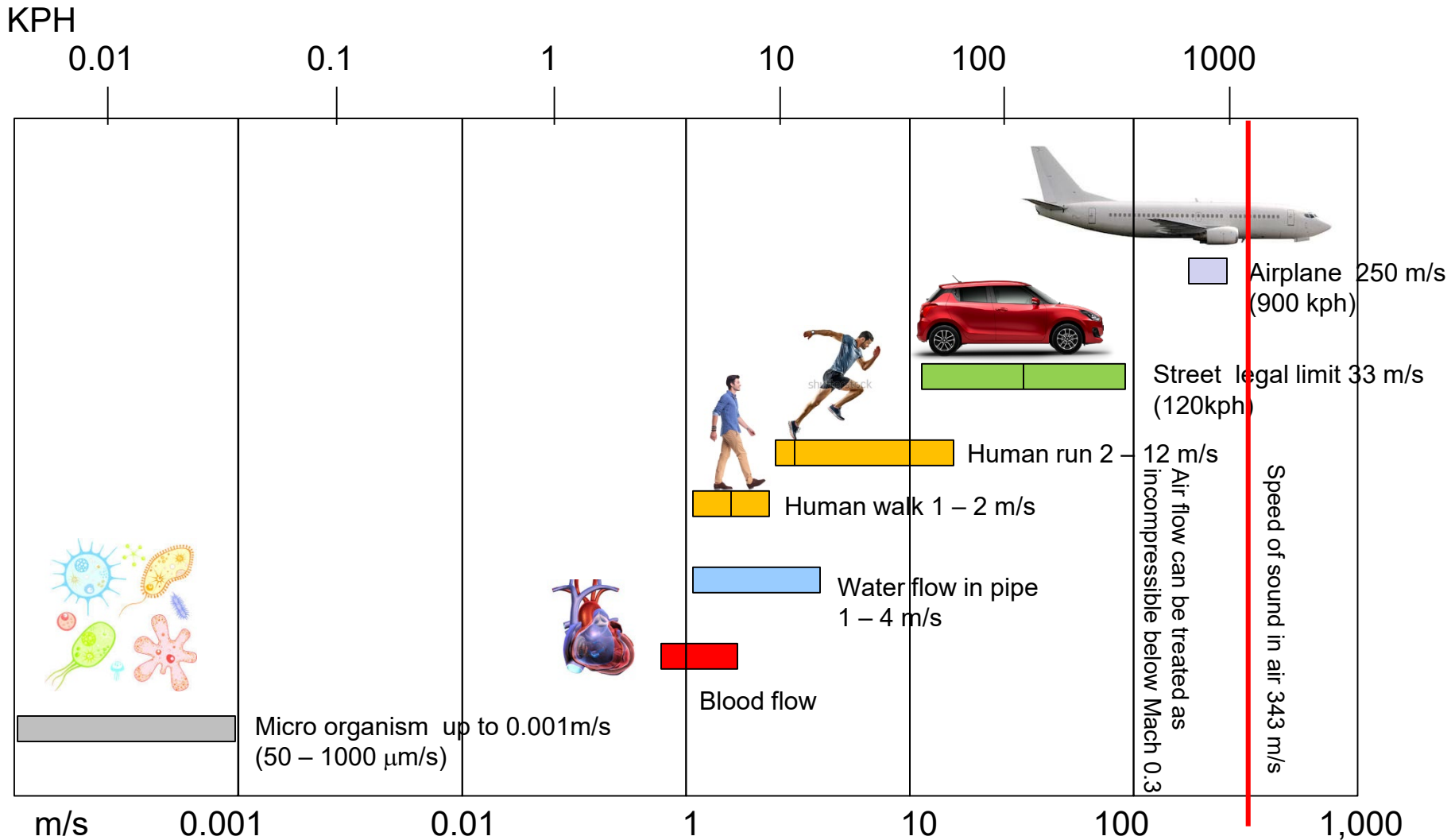


Velocity

foot/second, inch/second, meter/second, kilometer/hour, knot, mile/hour, nautical mile per hour

- 1 ft/s = 0.3048 m/s
- 1 ft/min = 5.08×10^{-3} m/s = 0.0183 km/h = 0.0114 mph
- 1 mph = 0.44703 m/s = 1.609 km/h = 88 ft/min = 5280 ft/hr = 1.467 Ft./sec. = 0.8684 knots
- 1 m/s = 3.6 km/h = 196.85 ft/min = 2.237 mph
- 1 km/h = 0.2778 m/s = 54.68 ft/min = 0.6214 mph = 0.5396 knot
- 1 knot (nautical mile per hour) = 0.514444444 m/s = 1.852 kilometers per hour = 1.1515 miles per hour = 1 nautical miles per hour

Velocity

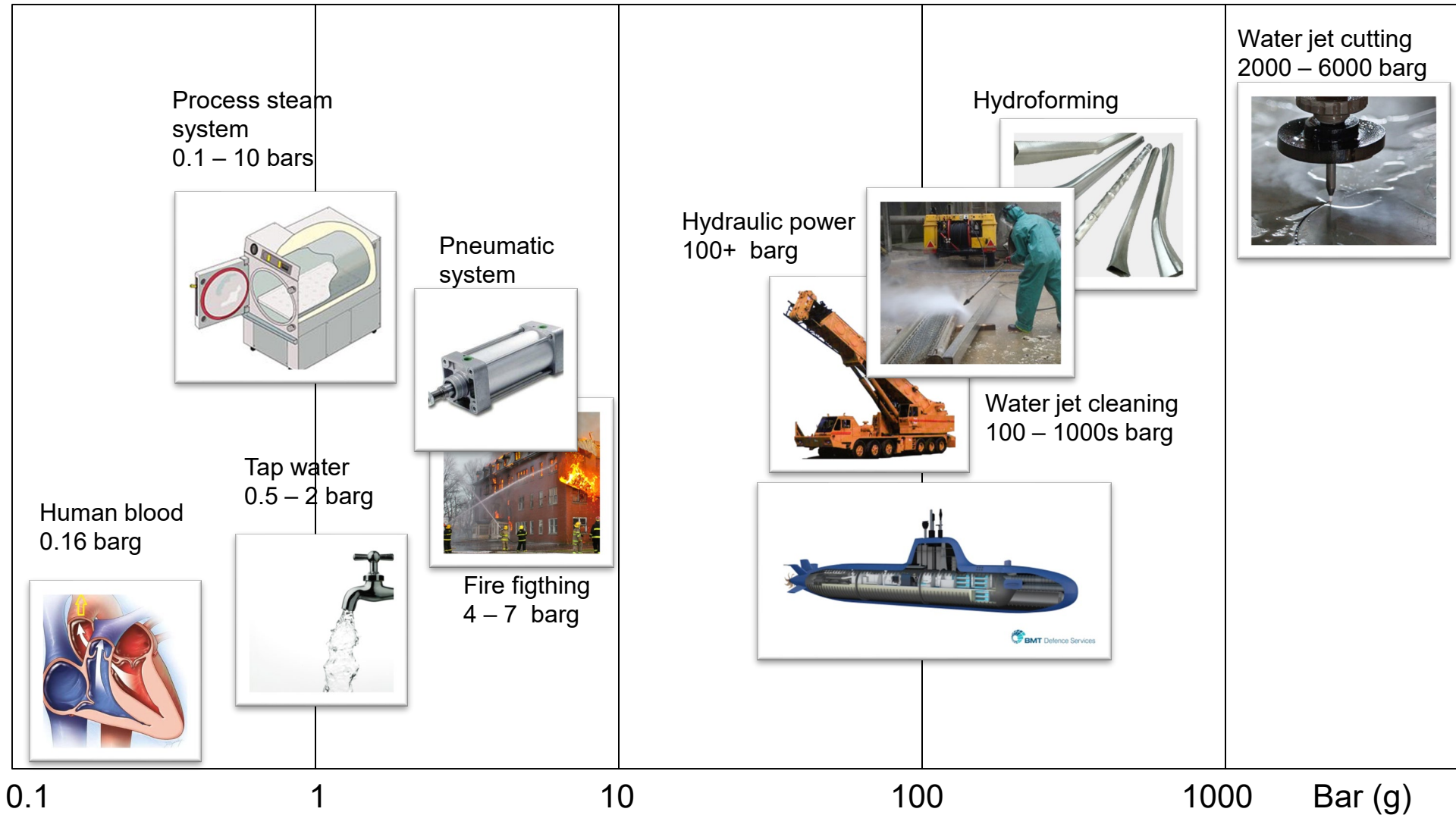


Pressure

atmosphere, centimeters of mercury, foot of water, bar, barye, centimeter of water, dyne/centimeter², inch of mercury, inch of water, kgf/centimeter², kgf/meter², lbf/foot², lbf/inch² (psi), millibar, millimeter of mercury, pascal, torr, newton/meter²

- Standard Atmospheric Pressure 1 atm = 101.325 kN/m² = 101.325 kPa = 14.7 psia = 0 psig = 29.92 in Hg = 760 torr = 33.95 Ft.H₂O = 407.2 In.W.G (Water Gauge) = 10.33 m.WG. = 2116.8 Lbs./Sq.Ft.
- 1 bar = 10⁵ Pa (N/m²) = 0.1 N/mm² = 10,197 kp/m² = 10.20 m H₂O = 0.9869 atm = 14.50 psi (lb_f/in²) = 10⁶ dyn/cm² = 750 mmHg
- 1 psi (lb/in²) = 144 psf (lb_f/ft²) = 6,894.8 Pa (N/m²) = 6.895x10⁻³ N/mm² = 6.895x10⁻² bar

Pressure Level (GAGE)



Energy

British Thermal Unit (Btu), calorie, joule, kilojoule, electron volt, erg, foot lb_f, foot poundal, kilocalorie, kilowatt hour, watt hour

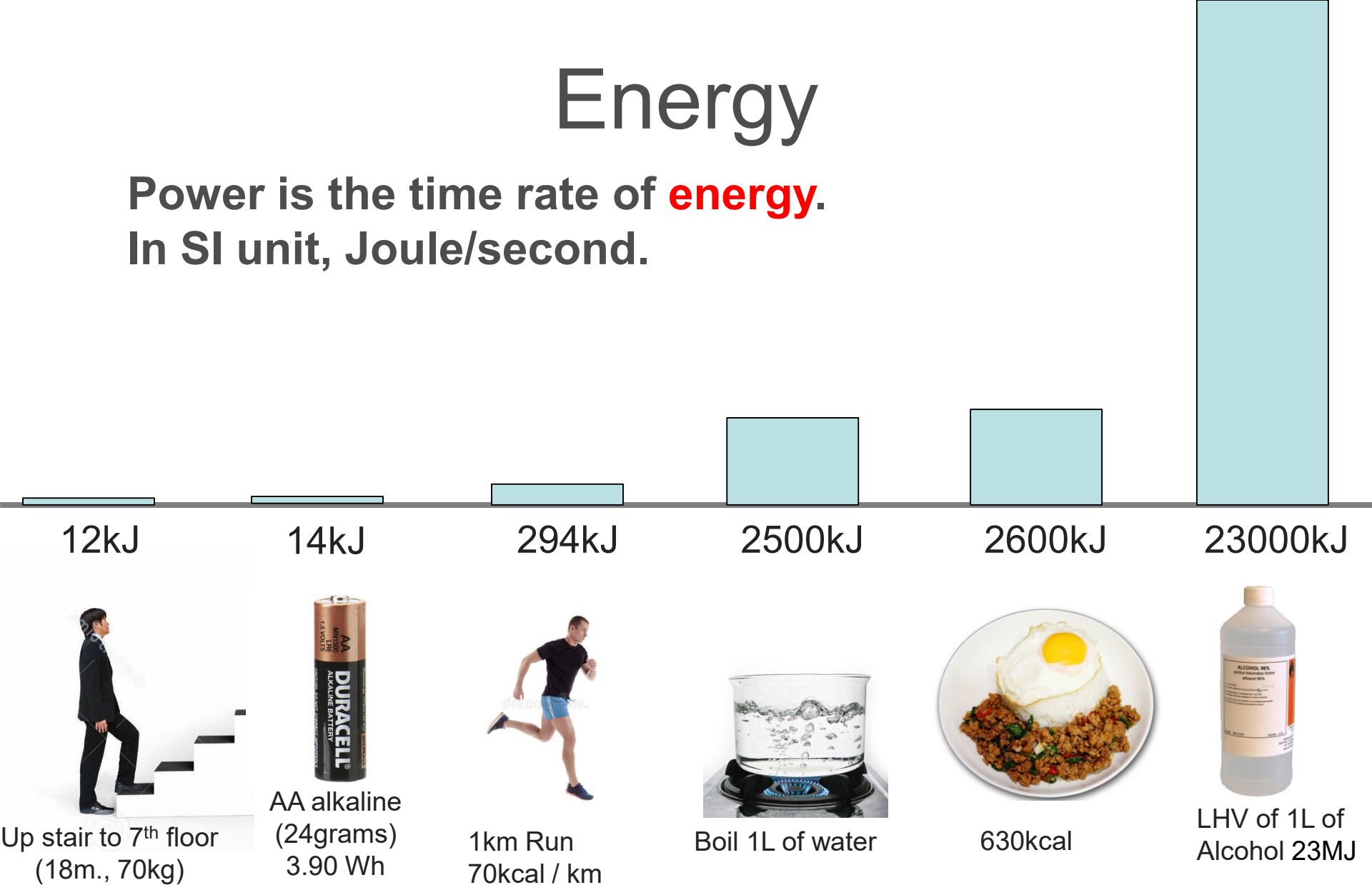
1 Btu = ความร้อนที่ต้องใช้ในการเพิ่มอุณหภูมิของน้ำ 1 ปอนด์ ขึ้น 1°F (58.5 °F ถึง 59.5 °F) ที่ระดับน้ำทะเล (ความดัน 30 in.HG.).

1 calorie = ความร้อนที่ต้องใช้ในการเพิ่มอุณหภูมิของน้ำ 1 กรัม ขึ้น 1°C

- $1 \text{ kWh} = 3.6 \times 10^6 \text{ J} = 3.671 \times 10^5 \text{ kpm} = 859.9 \text{ kcal} = 2.656 \times 10^6 \text{ ft lb}_f = 3.412 \times 10^3 \text{ Btu}$
- $1 \text{ kJ} = 1 \text{ kNm} = 1 \text{ kW s} = 10^3 \text{ J} = 0.947813 \text{ Btu} = 737.6 \text{ ft lb}_f = 0.23884 \text{ kcal}$
- $1 \text{ Btu (British thermal unit)} = 1,055.06 \text{ J} = 107.6 \text{ kpm} = 2.931 \times 10^{-4} \text{ kWh} = 0.252 \text{ kcal} = 778.16 \text{ ft lb}_f = 1.055 \times 10^{10} \text{ ergs} = 252 \text{ cal} = 0.293 \text{ watt hour}$
- $1 \text{ cal} = 4.186 \text{ J}$

Energy

Power is the time rate of **energy**.
In SI unit, Joule/second.



Heat Flowrate and Power

- 1 kW = 1,000 Watts = 3,412 Btu/h = 737.6/550 British hp = 1.341 British hp = $10^3/9.80665$ kg_f m/s = 737.6 ft lb_f/s = $10^3/(9.80665 \cdot 75)$ metric hp
- 1 hp (English horse power) = 745.7 W = 0.746 kW = 550 ft lb/s = 2,545 Btu/h = 33.000 ft lb/m = 1.0139 metric horse power $\approx$ 1.0 KVA
- 1 metric horse power = 736 W = 75 kg m/s = 0.986 English horse power
- 1 refrigeration Ton = 12,000 Btu/h cooling = 3.516 kW = 3,025.9 k Calories/h
- 1 Therm = 100,000 Btu/h
- 1 ft lb/s = 1.3558 W
- 1 Btu/s = 1055.1 W
- 1 Btu/h = 1 Btuh = 0.293 W = 0.001 MBH
- 1 Boiler Horse Power = 33,475.35 Bth/h = 9.81 kW

Viscosity

Viscosity dynamic (ความหนืด) – μ ความหนืดสัมบูรณ์

- $1 \text{ lb/(ft s)} = 1.4879 \text{ Pa s} = 14.88 \text{ P} = 1,488 \text{ cP} = 0.1517 \text{ kp s/m}^2$
- $1 \text{ cP (Centipoise)} = 10^{-3} \text{ Pa s} = 0.01 \text{ P} = 1.020 \times 10^{-4} \text{ kp s/m}^2 = 6.721 \times 10^{-4} \text{ lb/(ft s)} = 0.00100 \text{ (N s)/m}^2$
- $1 \text{ kg/(m s)} = 1 \text{ (N s)/m}^2 = 0.6720 \text{ lb}_m\text{/(ft s)} = 10 \text{ Poise}$
- $1 \text{ P (Poise)} = 0.1 \text{ Pa s} = 100 \text{ cP} = 1.020 \times 10^{-2} \text{ kp s/m}^2 = 6.721 \times 10^{-2} \text{ lb/(ft s)} = 0.1 \text{ kg/ms}$
- $1 \text{ Pa s (N s/m}^2) = 10 \text{ P (Poise)} = 10^3 \text{ cP} = 0.1020 \text{ kp s/m}^2 = 0.6721 \text{ lb/(ft s)}$
- $1 \text{ kp s/m}^2 = 9.80665 \text{ Pa s} = 98.07 \text{ P} = 9,807 \text{ cP} = 6.591 \text{ lb/(ft s)}$
- $1 \text{ reyns} = 1 \text{ lb}_f \text{ s/in}^2 = 6894.76 \text{ Pa s}$

Unit of Viscosity

Absolute or Dynamics viscosity, μ

$$\tau = \mu \frac{du}{dy} \quad \Rightarrow \quad \mu = \frac{\tau}{\left(\frac{du}{dy} \right)} \quad \Rightarrow \quad \text{Pa.s}$$

Diagram illustrating the derivation of the unit of viscosity (μ) from the shear stress equation $\tau = \mu \frac{du}{dy}$.

The equation is rearranged to $\mu = \frac{\tau}{\left(\frac{du}{dy} \right)}$.

Units are assigned to the terms:

- τ (shear stress) is in Pa (Pascals).
- $\frac{du}{dy}$ (velocity gradient) is in m/s (meters per second).
- y (distance) is in m (meters).

The final unit for viscosity is Pa.s (Pascal-seconds).

$$10^{-3} \text{ Pa.s} = 1 \text{ cP (centipoise)}$$

Properties of Some Fluids (approx.)

Fluids (Temp.)	Density (kg/m ³)	Absolute Viscosity (Pa-s)
Air (30C)	1.16	18.6×10^{-6}
Water (30C)	996	0.798×10^{-3}
Sea water (30C)	1022	0.86×10^{-3}
Bloods (37C)	1060	2.8×10^{-3}
Ethanol (30C)	781	0.983×10^{-3}
Kerosine (30C)	820	1.4×10^{-3}
SAE 10W-30 Oil (30C)	840	0.09
Glycerin (30C)	1260	0.6
Mercury (30C)	13496	1.45×10^{-3}

Kinematic Viscosity

Kinematic viscosity (ν)

$$\nu = \frac{\mu}{\rho}$$

Units of kinematic viscosity are in m^2/s or Stoke

$$1 \text{ St (Stokes)} = 10^{-4} \text{ m}^2/\text{s} = 1 \text{ cm}^2/\text{s}$$

Since the *Stoke* is a large unit it is often divided by 100 into the smaller unit **centiStoke (cSt)** - where

- $1 \text{ St} = 100 \text{ cSt}$
- $1 \text{ cSt (centiStoke)} = 10^{-6} \text{ m}^2/\text{s} = 1 \text{ mm}^2/\text{s}$
- $1 \text{ m}^2/\text{s} = 10^6 \text{ centiStokes}$

Viscosity

Viscosity kinematic (ความหนืดเชิงจลนศาสตร์) – $\nu = (\mu / \rho)$

- $1 \text{ ft}^2/\text{s} = 0.0929 \text{ m}^2/\text{s}$
- $1 \text{ ft}^2/\text{h} = 2.581 \times 10^{-5} \text{ m}^2/\text{s}$
- $1 \text{ St (Stokes)} = 1 \times 10^{-4} \text{ m}^2/\text{s} = 100 \text{ cSt} = 1.076 \times 10^{-3} \text{ ft}^2/\text{s}$
- $1 \text{ m}^2/\text{s} = 10^4 \text{ St} = 10^6 \text{ cSt} = 10.764 \text{ ft}^2/\text{s} = 38750 \text{ ft}^2/\text{h}$
- $1 \text{ cSt (Centistokes)} = 10^{-6} \text{ m}^2/\text{s} = 0.01 \text{ St} = 1.076 \times 10^{-5} \text{ ft}^2/\text{s}$

Water Properties

อุณหภูมิ T (°C)	ความหนาแน่น ρ kg/m ³	Dynamic Viscosity μ (N.s/m ²) x 10 ⁻³	Kinematic Viscosity ν (x 10 ⁻⁶ m ² /s) *	ความดันไอ (kPa)**
0 (น้ำแข็ง)	916.2			
0	999.9	1.787	1.787	0.87
5	1000	1.519	1.519	0.92
10	999.7	1.307	1.307	1.18
20	998.2	1.002	1.004	2.29
30	995.7	0.798	0.801	4.27
40	992.2	0.653	0.658	7.43
50	988.1	0.547	0.553	12.36
60	983.2	0.467	0.475	19.89
70	977.8	0.404	0.413	31.10
80	971.8	0.355	0.365	47.32
90	965.3	0.315	0.326	70.16
100	958.4	0.282	0.294	101.3
100 (ไอน้ำ)	0.598			

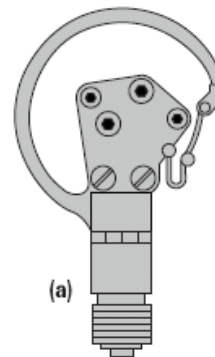
* $1 \times 10^{-6} \text{ m}^2/\text{s} = 1 \text{ Centistroke}$

** $1 \text{ bar} = 100 \text{ kPa}$

GUAGE PRESSURE

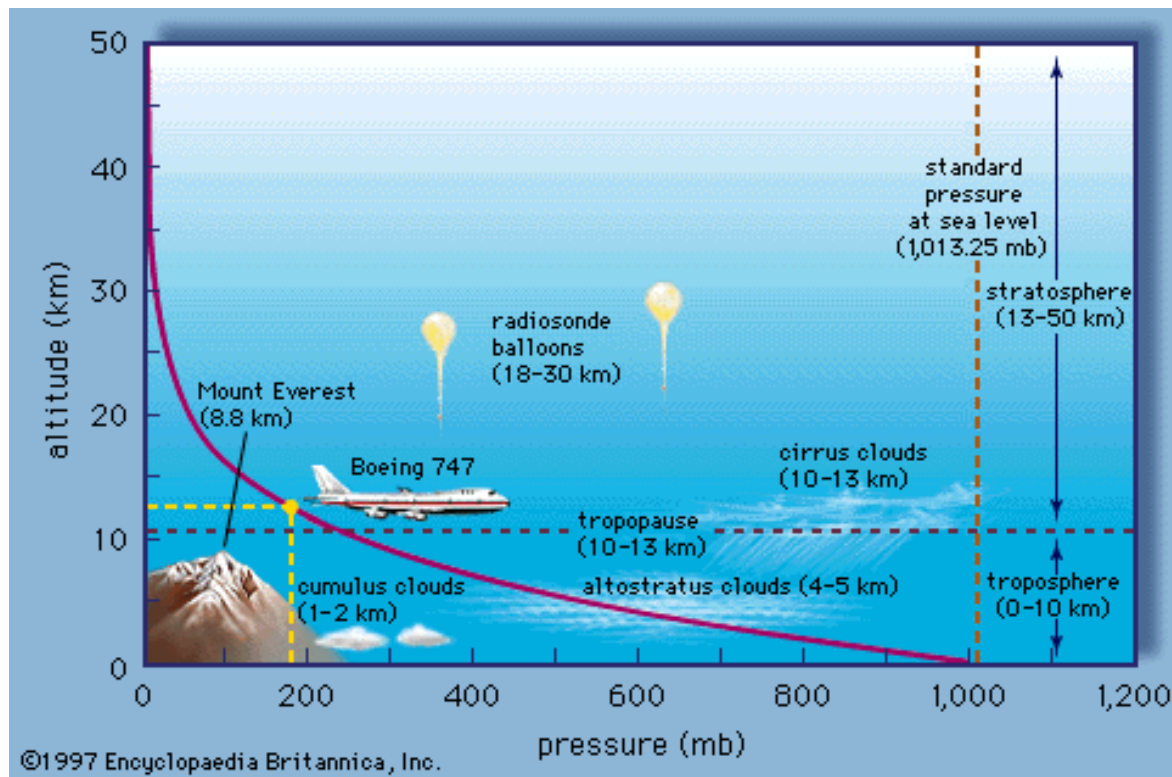
$$P_{\text{guage}} = P_{\text{absolute}} - P_{\text{atm}}$$

P_{guage} is obtained from pressure measuring device.



Atmospheric pressure

P_{atm} varies with altitude

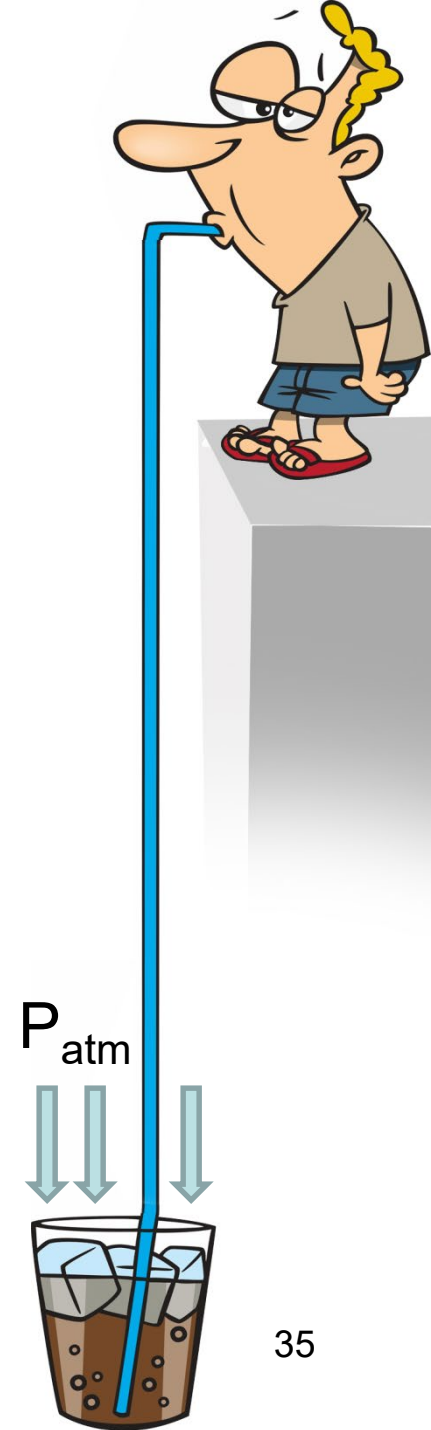


Pressure at sea level

At sea level $P_{\text{atm}} = 101.3 \text{ kPa}$ $P = \rho gh$

Water can be drawn upto

$$h = P_{\text{atm}} / \rho_{\text{water}} g = ?? \text{ m}$$



Pressure and elevation

- In theory 1 barg of pressure can drive water up 10.2 m with zero flow.
- Waterworks Authority (MWA/PWA) attempt to deliver water at 1-2 barg.
- 2 barg = 20.4 m.WG. → = 6 Floors !!
- In practical situations, pressure drops in main and branch pipes, water hardly reach 2nd floor, so people use pump.

City Water Pressure

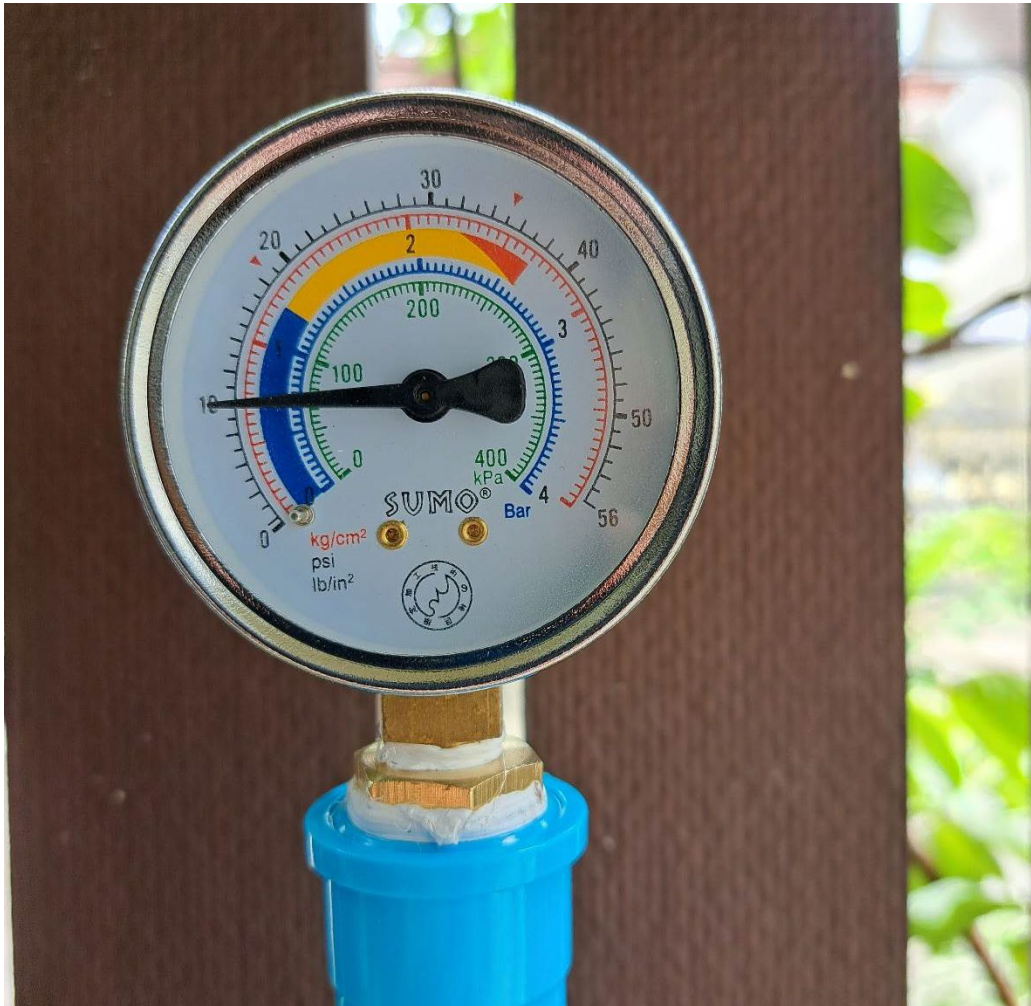
Rocket
Media
Lab

แรงดันน้ำประปา

ประเทศไทยไม่มีการกำหนดแรงดันขั้นต่ำของน้ำประปา จึงใช้ค่าแรงดันของท่อประปาแทน



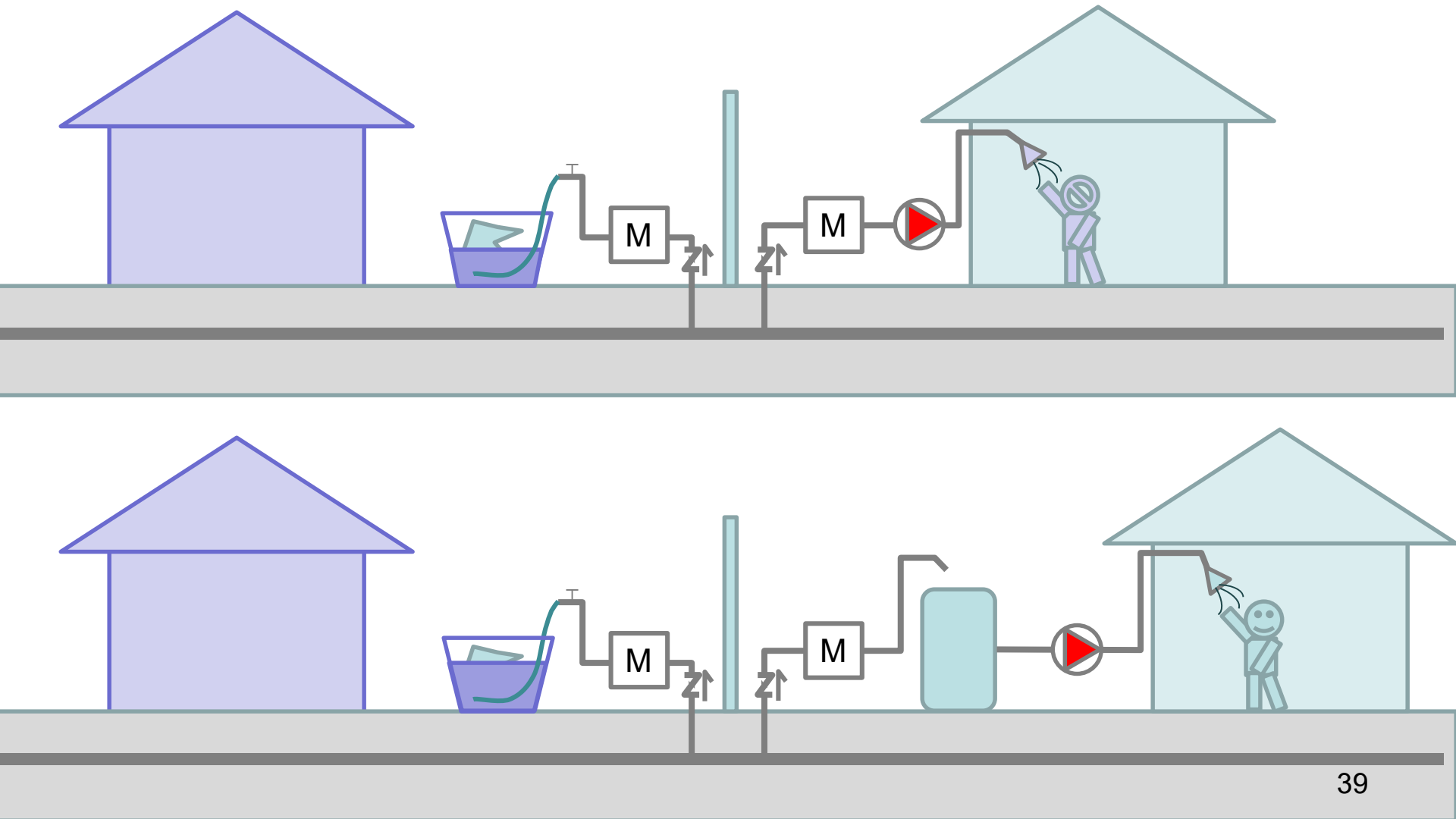
Water pressure from PWA



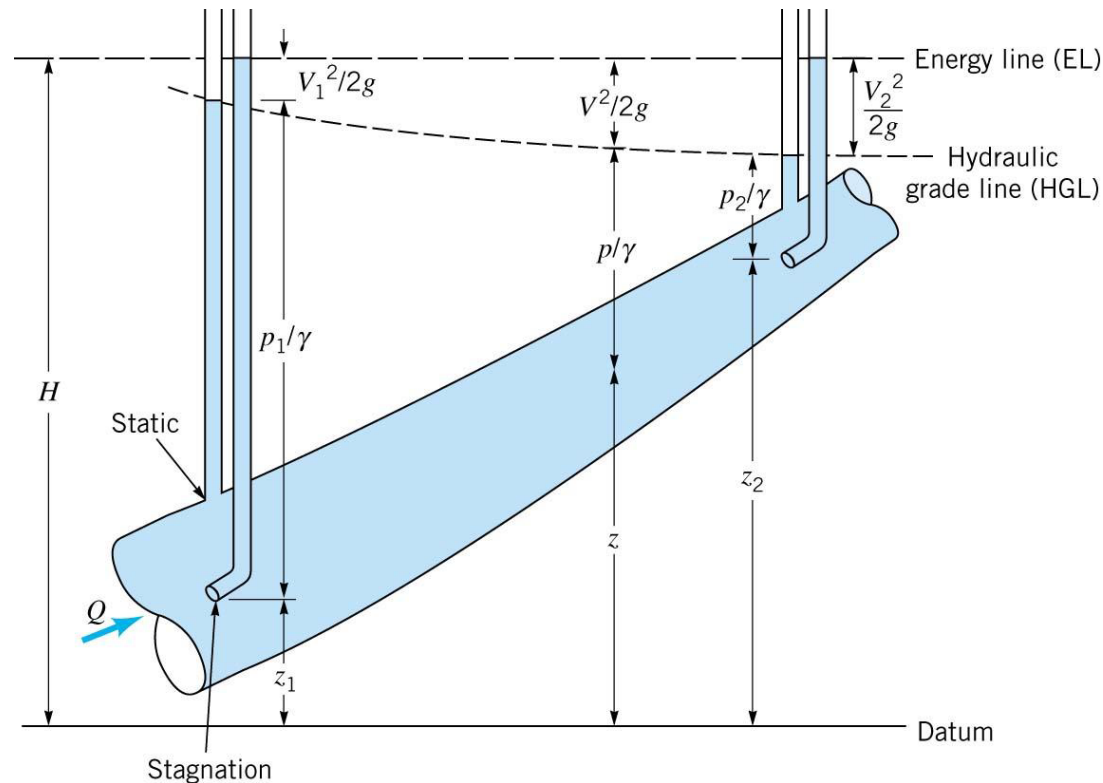
8 Aug 2022
Klong Luang
Patumthani



It's illegal to pump water from city main



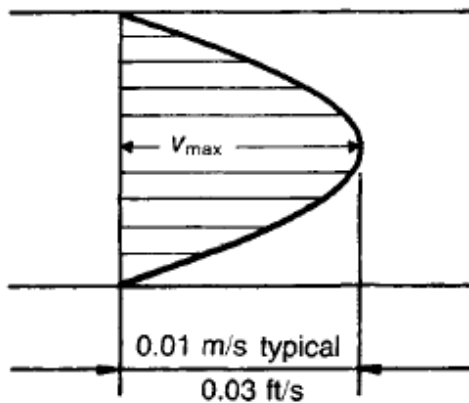
4. BASIC FLOW IN PIPE



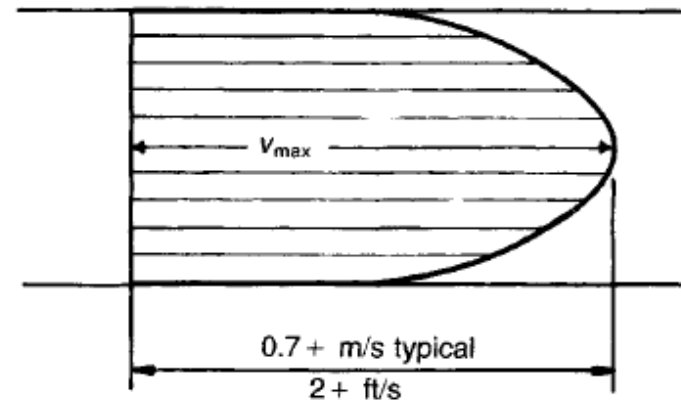
$$\frac{p_1}{\rho g} + \frac{V_1^2}{2g} + z_1 = \frac{p_2}{\rho g} + \frac{V_2^2}{2g} + z_2 + LOSS$$

Flow Pattern

LAMINAR or TURBULENCE ?



$Re < 2000$



$Re > 10000$

REYNOLDS NUMBER

$$Re = \frac{vD}{\nu}$$

Inertia vs. Viscous Effect

WATER FLOW AT 1.2 m/s IN A ½" PIPE

$$Re = \frac{1.2 \cdot 0.0125}{10^{-6}} = 15000$$

=TURBULENT

LOSS

MAJOR LOSS: LOSS IN PIPE

MINOR LOSS: LOSS IN FITTINGS AND VALVES

"K" FACTOR TABLE—SHEET 2 of 4

REPRESENTATIVE RESISTANCE COEFFICIENTS (K) FOR VALVES AND FITTINGS

(For formulas and friction data, see page 52)

(*K* is based on use of schedule pipe as listed on page 52)

GATE VALVES

Wedge Disc, Double Disc, or Plug Type

If: $\beta = 1$, $\theta = 0^\circ \dots K_1 = 8 f_r$
If: $\beta < 1$ and $\theta \neq 45^\circ \dots K_1 = \text{Formula 5}$
If: $\beta < 1$ and $45^\circ < \theta \leq 180^\circ \dots K_1 = \text{Formula 6}$

SWING CHECK VALVES

$K = 100 f_r$
Minimum pipe velocity (fps) for full disc lift
 $= 35 \sqrt{V}$

$K = 50 f_r$
Minimum pipe velocity (fps) for full disc lift
 $= 60 \sqrt{V}$
U.S. Liquid = $100 \sqrt{V}$

GLOBE AND ANGLE VALVES

If: $\beta = 1 \dots K_1 = 340 f_r$

If: $\beta = 1 \dots K_1 = 55 f_r$

If: $\beta = 1 \dots K_1 = 150 f_r$ If: $\beta = 1 \dots K_1 = 55 f_r$

All globe and angle valves,
whether reduced seat or threaded.

If: $\beta < 1 \dots K_1 = \text{Formula 7}$

LIFT CHECK VALVES

If: $\beta = 1 \dots K_1 = 100 f_r$
If: $\beta < 1 \dots K_1 = \text{Formula 7}$
Minimum pipe velocity (fps) for full disc lift
 $= 40 \beta \sqrt{V}$

If: $\beta = 1 \dots K_1 = 55 f_r$
If: $\beta < 1 \dots K_1 = \text{Formula 7}$
Minimum pipe velocity (fps) for full disc lift
 $= 340 \beta \sqrt{V}$

TILTING DISC CHECK VALVES

	STEEL	IRON
Sizes 3 to 8"	$K = 150 f_r$	$K = 150 f_r$
Sizes 10 to 14"	$K = 30 f_r$	$K = 30 f_r$
Sizes 16 to 48"	$K = 20 f_r$	$K = 20 f_r$
Minimum pipe velocity (fps) for full disc lift =	$80 \sqrt{V}$	$30 \sqrt{V}$

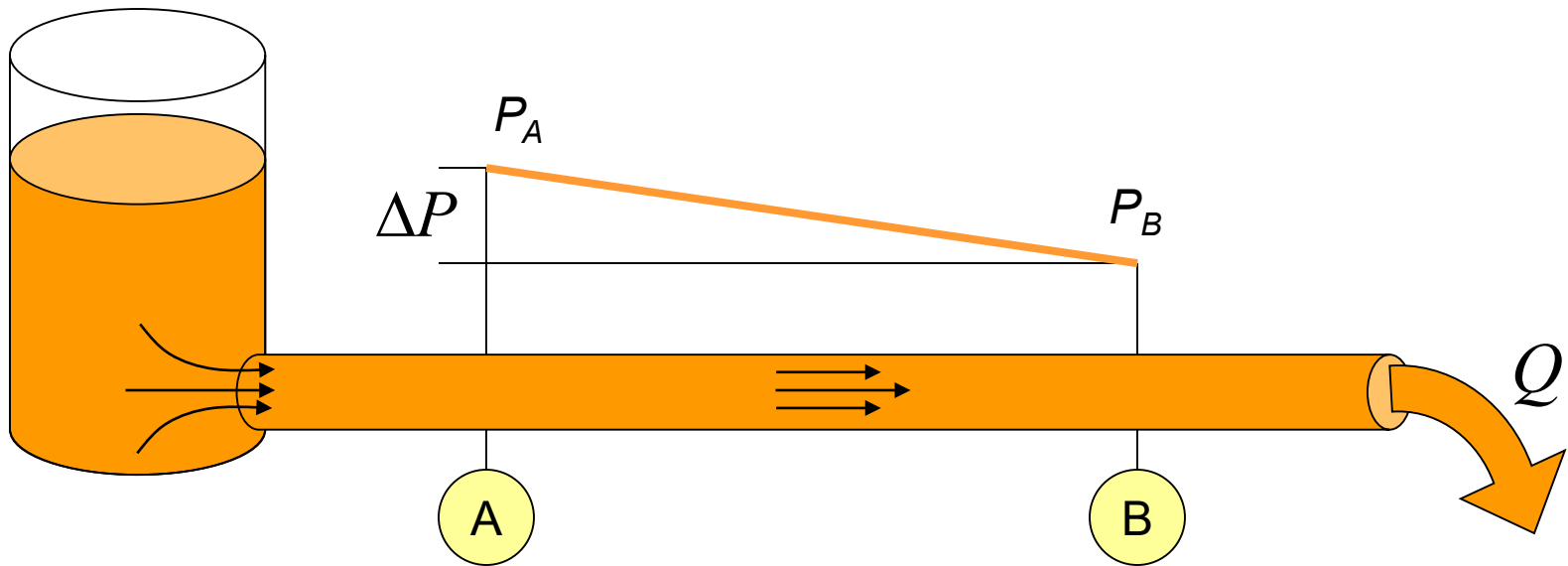
"K" FACTOR TABLE—SHEET 4 of 4
REPRESENTATIVE RESISTANCE COEFFICIENTS (K) FOR VALVES AND FITTINGS
(For formulas and friction data, see page 52)
(*K* is based on use of schedule pipe as listed on page 52)

PLUG VALVES AND COCKS		STANDARD ELBOWS																													
 Straight-Way If: $\beta = 1$, $K_1 = 18 f_r$ If: $\beta < 1 \dots K_1 = \text{Formula 6}$	 3-Way If: $\beta = 1$, $K_1 = 30 f_r$ If: $\beta < 1 \dots K_1 = 90 f_r$	 90° $K = 30 f_r$	 45° $K = 16 f_r$																												
MITRE BENDS		STANDARD TEES																													
	<table border="1"> <thead> <tr> <th>Angle</th> <th>K</th> </tr> </thead> <tbody> <tr><td>0°</td><td>2 f_r</td></tr> <tr><td>15°</td><td>4 f_r</td></tr> <tr><td>30°</td><td>6 f_r</td></tr> <tr><td>45°</td><td>15 f_r</td></tr> <tr><td>60°</td><td>25 f_r</td></tr> <tr><td>75°</td><td>40 f_r</td></tr> <tr><td>90°</td><td>60 f_r</td></tr> </tbody> </table>	Angle	K	0°	2 f _r	15°	4 f _r	30°	6 f _r	45°	15 f _r	60°	25 f _r	75°	40 f _r	90°	60 f _r	 Flow thru run $\dots K = 30 f_r$ Flow thru branch $\dots K = 60 f_r$													
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r/d	K	r/d	K																												
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CLOSE PATTERN RETURN BENDS		PIPE EXIT																													
 $K = 50 f_r$	Projecting $K = 1.0$ 	Sharp-Edged $K = 1.0$ 	Rounded $K = 1.0$ 																												

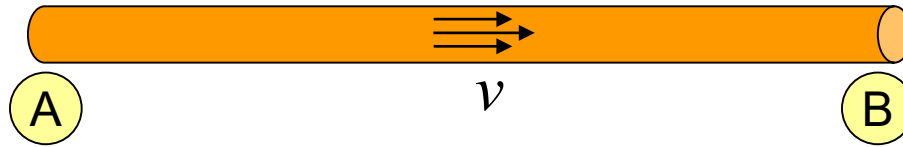
LOSS IN PIPE

LOSS IN PIPE CAUSED BY FRICTION BETWEEN FLUID AND PIPE SURFACE.
FRICTION CAN BE RELATED TO SHEAR STRESS.

$$\tau = \mu \frac{du}{dy}$$

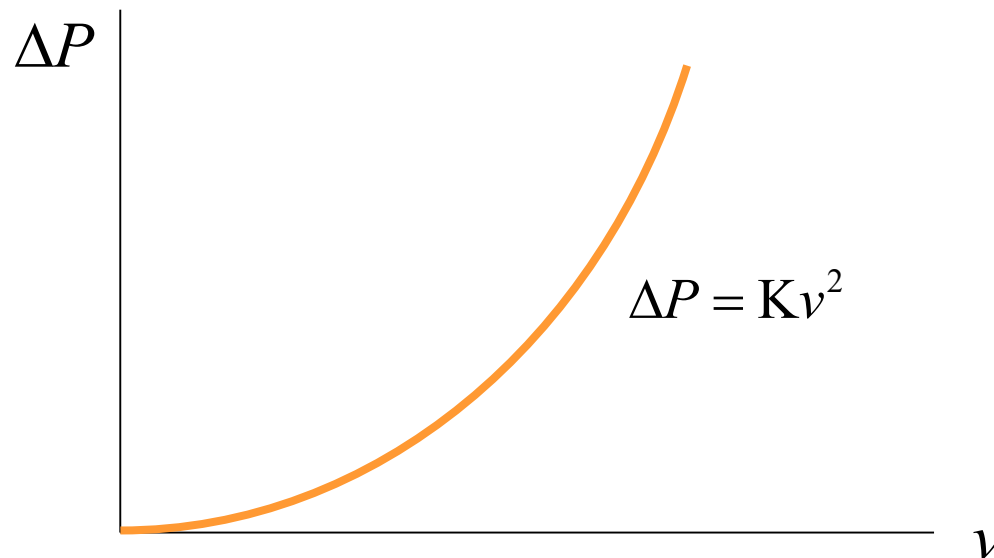


VELOCITY AND LOSS



LOSS IN PIPE VARIES WITH SQUARE
OF FLUID VELOCITY

$$\Delta P \propto v^2$$

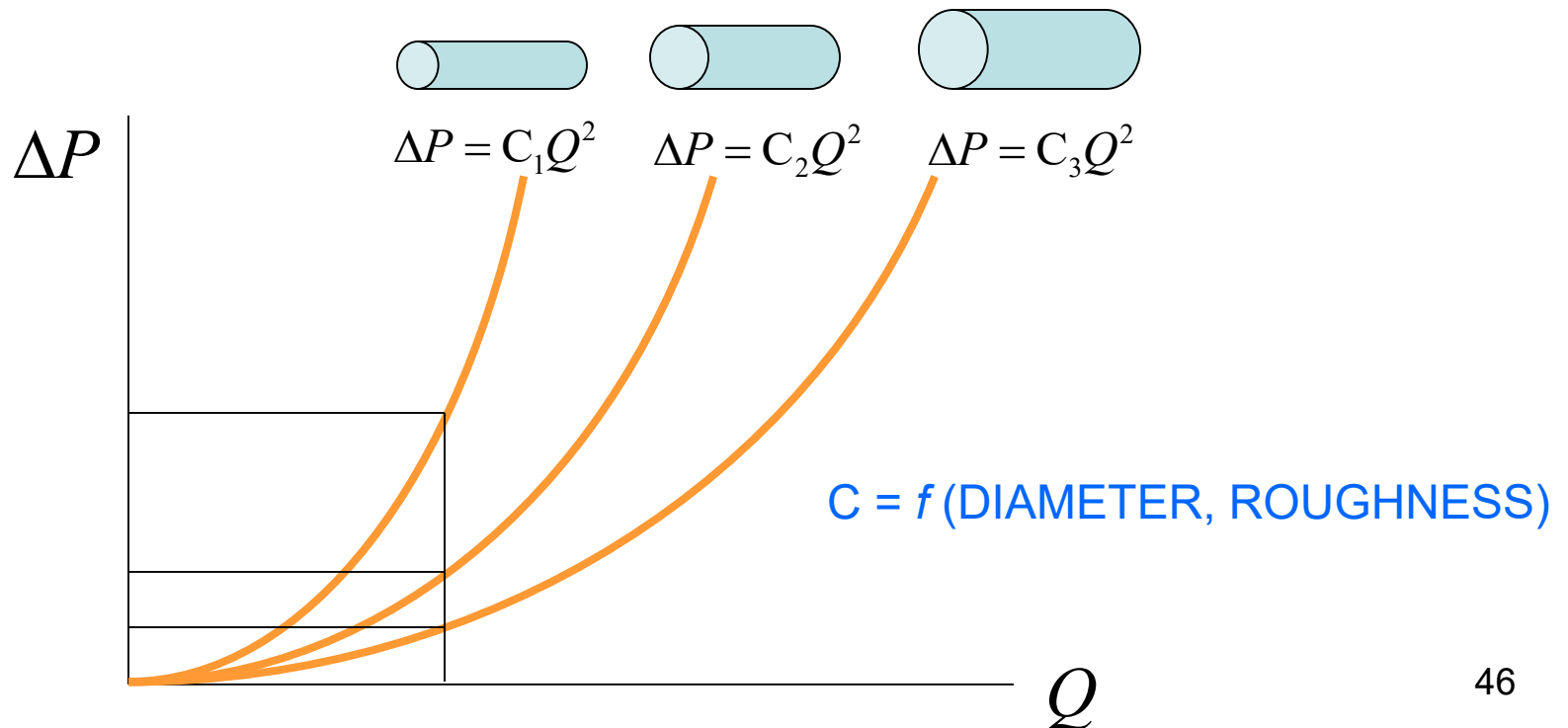


FLOW AND LOSS

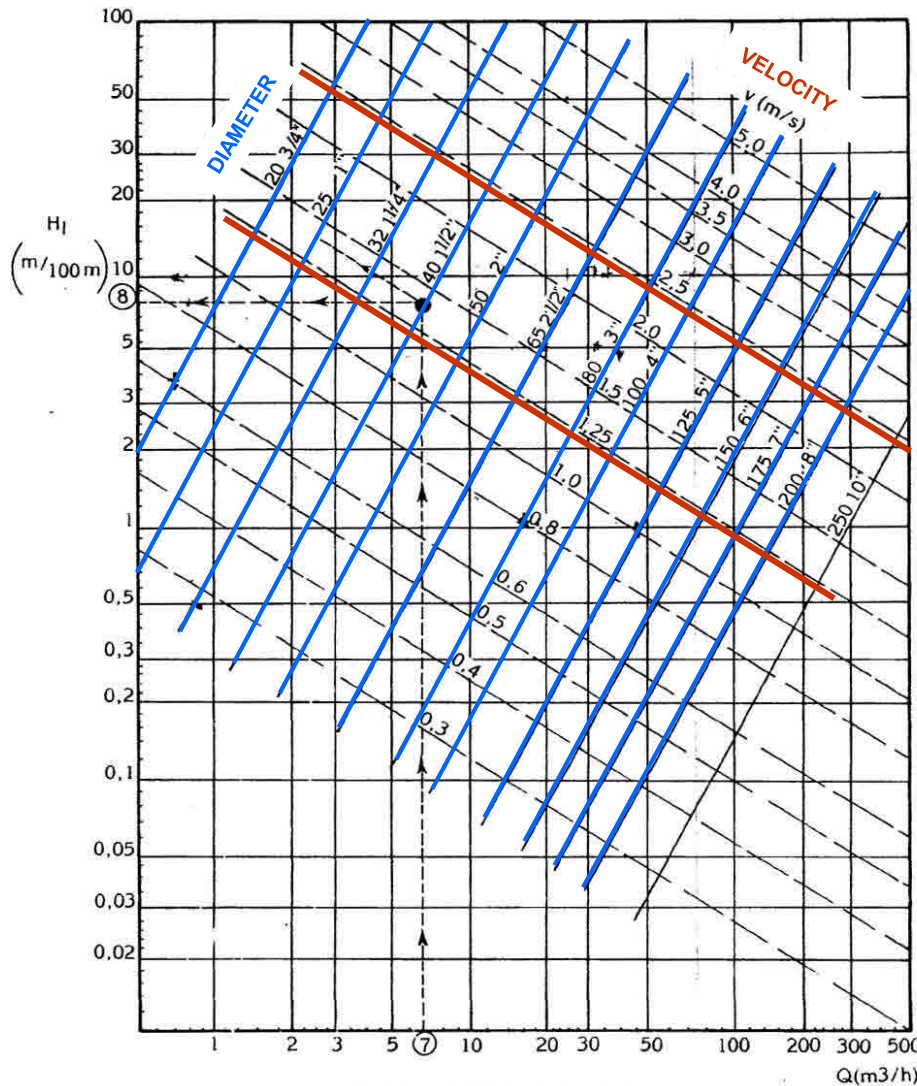
FLUID VELOCITY IS RELATED TO
THE FLOW RATE VIA PIPE SIZE

$$v = \frac{Q}{\left(\frac{\pi D^2}{4}\right)}$$

THUS.. $\Delta P \propto Q^2$



FRICTION LOSS CHART



DESIGN VELOCITY
1.2 TO 2.4 m/s

FRICTION LOSS EQUATION

HAZEN-WILLIAMS EQUATION (SI UNIT)

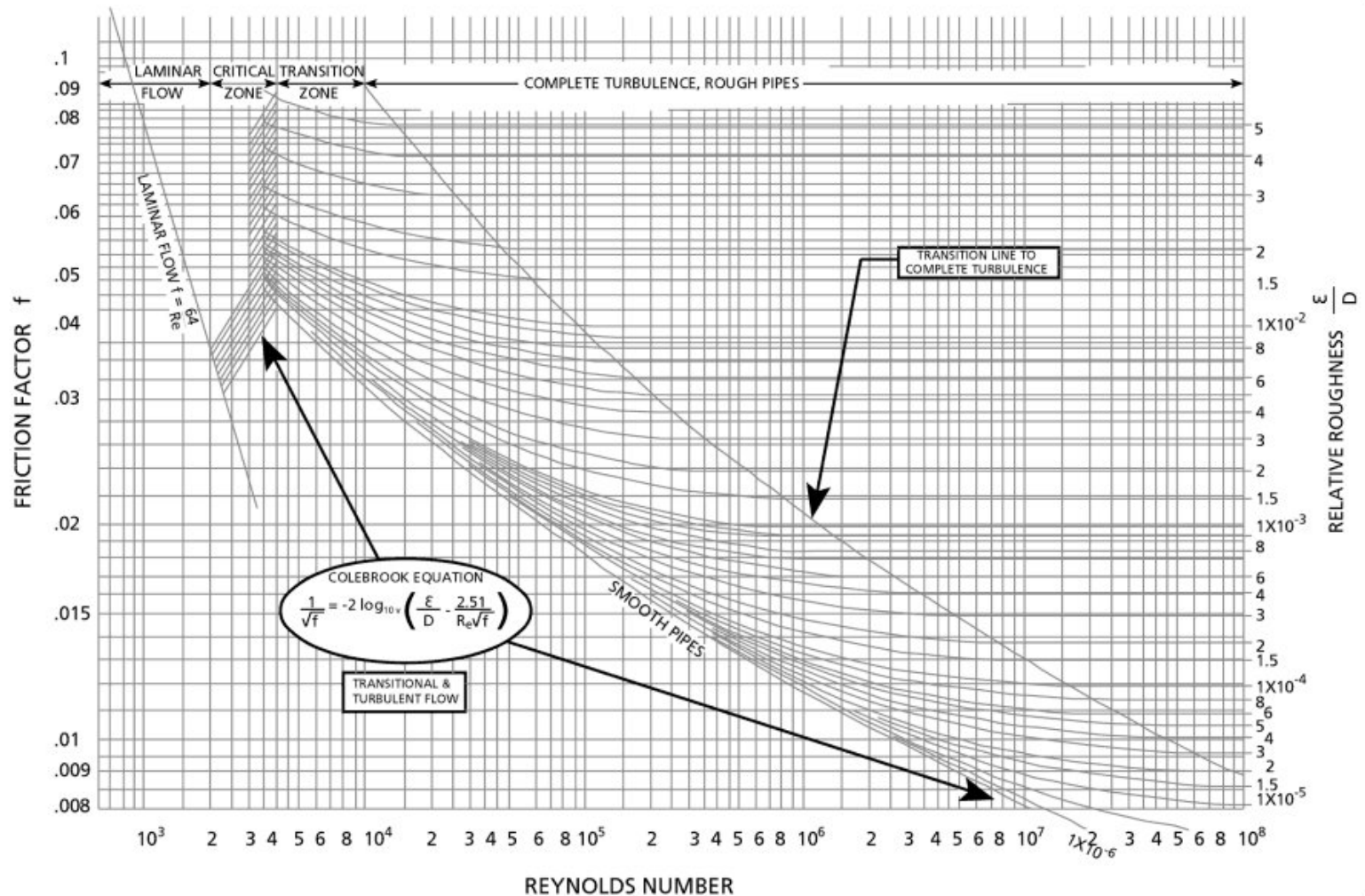
$$h_f = \left(\frac{151Q}{CD^{2.63}} \right)^{1.85}$$

DARCY WEISBACH EQUATION

$$h = f \frac{L}{D} \frac{v^2}{2g}$$

READING ASSIGNMENT: **3-2 FRICTION LOSS IN PIPE**

MOODY DIAGRAM



MINOR LOSS

LOSS IN FITTING: USE EQUIVALENT LENGTH

LOSS IN VALVE: USE C_v OR K_v

(DISCUSS LATER)

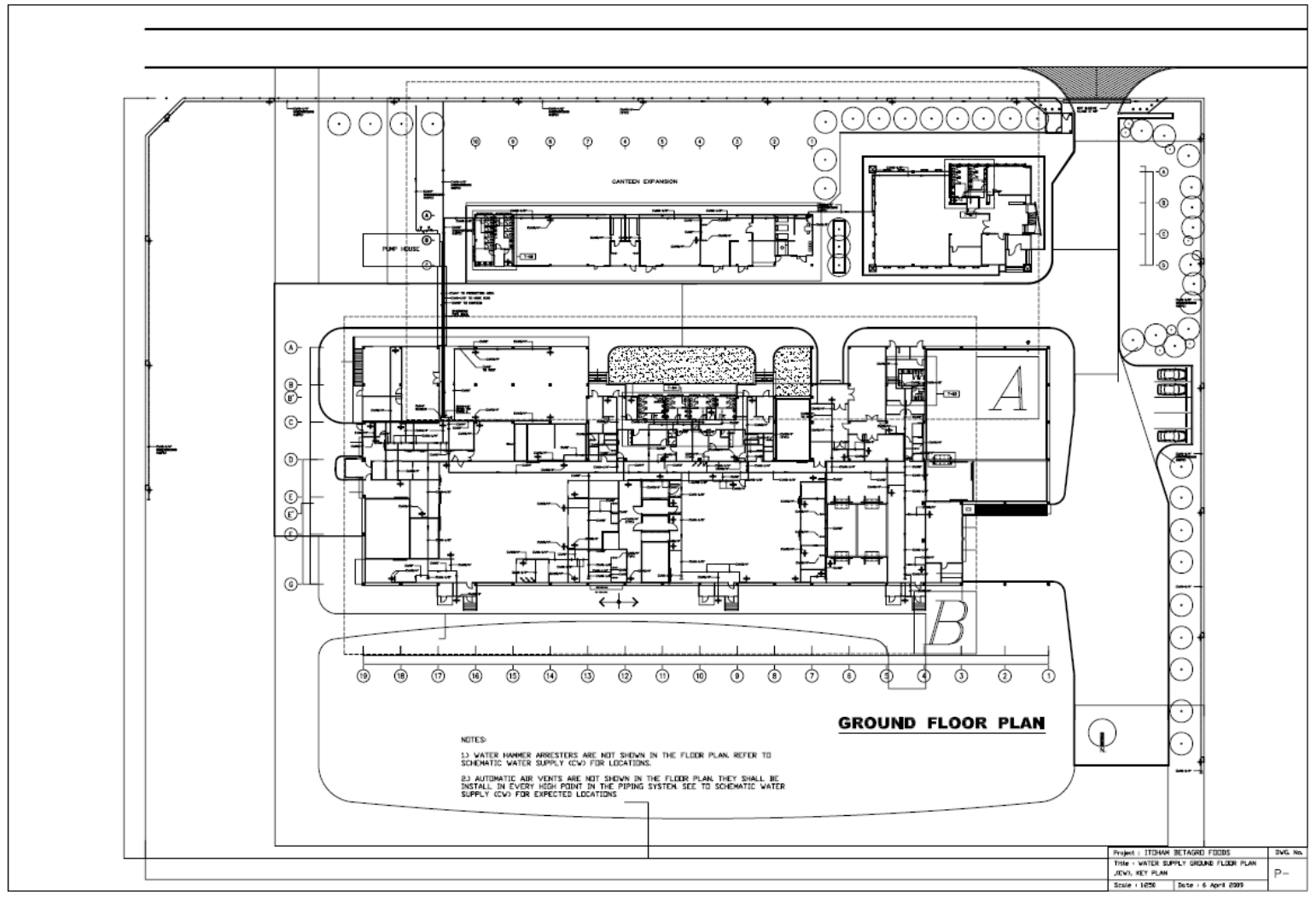
"K" FACTOR TABLE—SHEET 2 of 4
REPRESENTATIVE RESISTANCE COEFFICIENTS (K) FOR VALVES AND FITTINGS
(For formulas and friction data, see page 52)
(*K* is based on use of schedule pipe as listed on page 52)

GATE VALVES Wedge Disc, Double Disc, or Plug Type		SWING CHECK VALVES	
$K = 100 f_r$	$K = 10 f_r$	$K = 100 f_r$	$K = 10 f_r$
If: $\beta = 1$, $\theta = 0^\circ \dots K_1 = 8 f_r$ If: $\beta < 1$ and $\theta \neq 45^\circ \dots K_1 = \text{Formula 5}$ If: $\beta < 1$ and $45^\circ < \theta \leq 180^\circ \dots K_1 = \text{Formula 6}$		Minimum pipe velocity (fps) for full disc lift $= 55 \sqrt{V'} \quad \text{or} \quad \frac{10.4 \text{ L/min}}{\sqrt{V'}}$	
GLOBE AND ANGLE VALVES		LIFT CHECK VALVES	
$K = 100 f_r$	$K = 100 f_r$	$K = 100 f_r$	$K = 100 f_r$
If: $\beta = 1 \dots K_1 = 340 f_r$ If: $\beta = 1 \dots K_1 = 55 f_r$		Minimum pipe velocity (fps) for full disc lift $= 40 \sqrt{V'} \quad \text{or} \quad \frac{10.4 \text{ L/min}}{\sqrt{V'}}$	
All globe and angle valves, whether reduced seat or throttled. If: $\beta < 1 \dots K_1 = \text{Formula 7}$		TILTING DISC CHECK VALVES If: $\beta = 1 \dots K_1 = 150 f_r$ If: $\beta = 1 \dots K_1 = 55 f_r$	

"K" FACTOR TABLE—SHEET 4 of 4
REPRESENTATIVE RESISTANCE COEFFICIENTS (K) FOR VALVES AND FITTINGS
(For formulas and friction data, see page 52)
(*K* is based on use of schedule pipe as listed on page 52)

PLUG VALVES AND COCKS		STANDARD ELBOWS	
$K = 18 f_r$	$K = 10 f_r$	$K = 30 f_r$	$K = 10 f_r$
If: $\beta = 1$, $K_1 = 18 f_r$ If: $\beta < 1 \dots K_1 = \text{Formula 6}$		STANDARD TEES Flow thru run $\dots K = 30 f_r$ Flow thru branch $\dots K = 60 f_r$	
MITRE BENDS		PIPE ENTRANCE	
$K = 10 f_r$	$K = 10 f_r$	$K = 0.75$	$K = 0.75$
90° PIPE BENDS AND FLANGED OR BUTT-WELDING 90° ELBOWS The resistance coefficient, K_B , for pipe bends other than 90° may be determined as follows: $K_B = (n - 1) \left(0.25 \pi f_r \frac{L}{D} + 0.5 K \right) = K$ n = number of 90° bends K = resistance coefficient for one 90° bend (see table)		PIPE EXIT Projecting $K = 1.0$ Sharp-Edged $K = 1.0$ Rounded $K = 1.0$	

5. QUICK LOOK AT PIPE DRAWINGS



NEXT SESSION

PIPING MATERIALS AND EQUIPMENTS

VALVES

PUMPS

HOMework 1

- Find a water valve (for example, in a toilet, a kitchen or the backyard).
- Measure inlet pipe size. Draw or photograph the valve.
- Measure the flow rate in LPM from the valve at various valve opening positions (for example 25%, 50%, 75% and 100%).
- Find out the supply pressure (in m.WG.)
- Plot flowrate vs % open

